

Pilot-scale Evaluation of High-Temperature-Winkler® Gasification using Waste Wood as Feedstock

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Crude oil



Coal



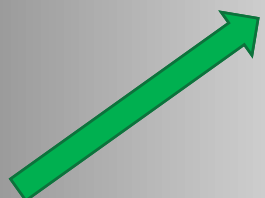
Fuels



Chemicals



Biomass

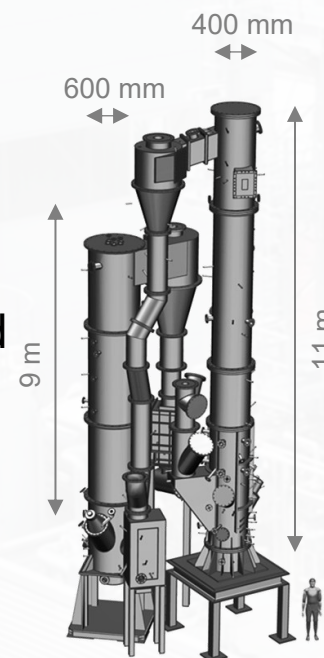


gasifier island

High-Temperature-Winkler® (HTW®) -
gasification
(~ 450 kW_{th})

Circulating Fluidized
Bed-Gasification
(~ 1 MW_{th})

Chemical Looping-
Gasification
(~ 1 MW_{th})

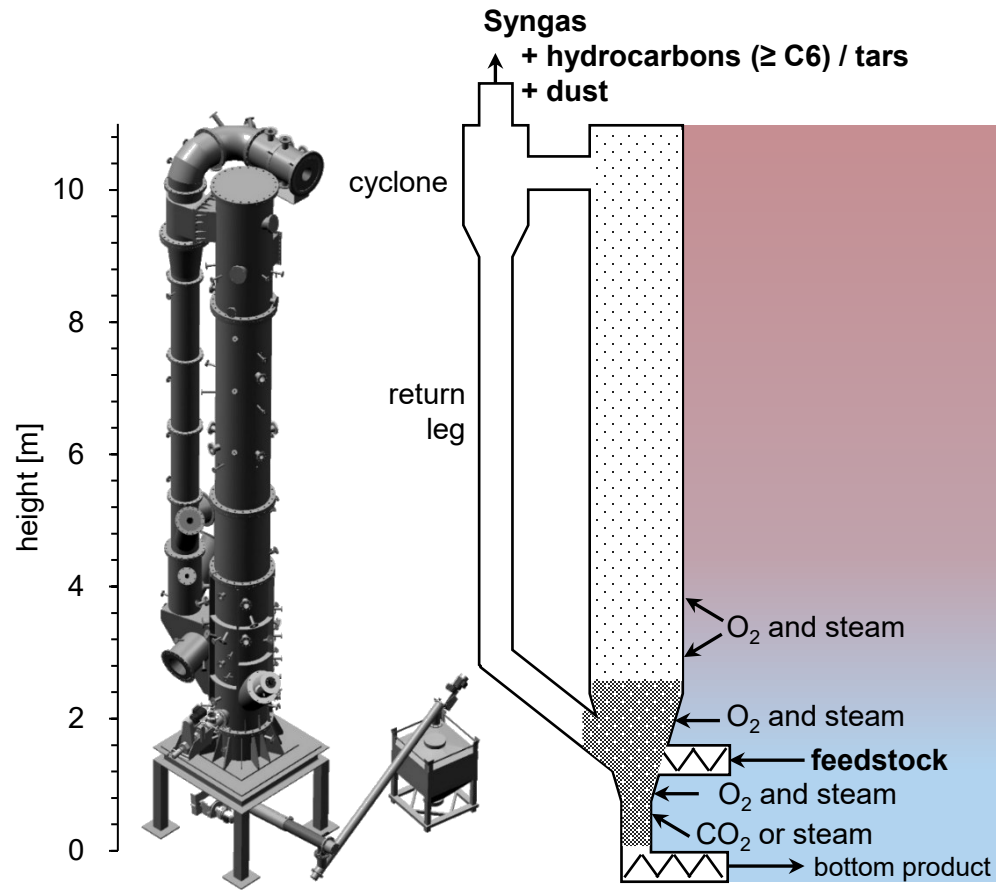


gas cleaning



synthesis

HTW®-Gasifier



Post gasification zone (PGZ) – 800 to 1100 °C

- freeboard
- conversion of hydrocarbons
- conversion of fixed carbon (entrained dust)

Bubbling bed – 650 to 750 °C

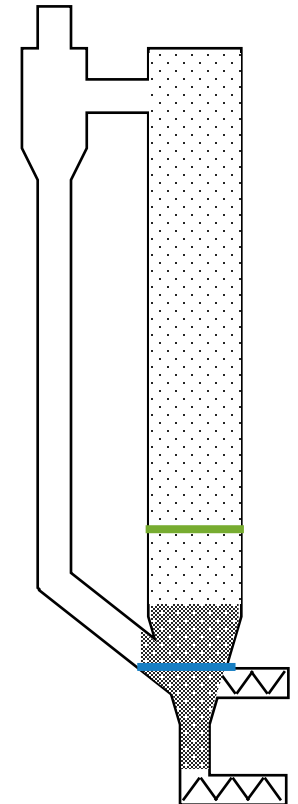
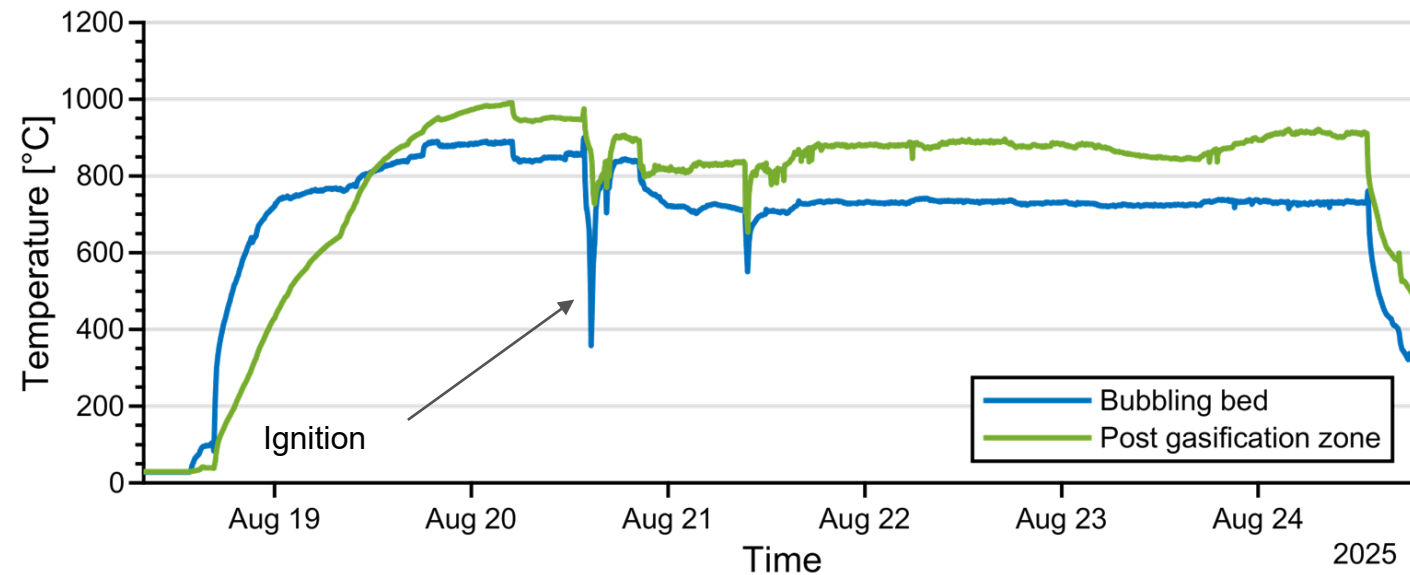
- homogeneous temperature profile
- release of volatiles & conversion of fixed carbon
- bed inventory: ash and char
- temperature below ash softening point



HTW® Gasification



Waste Wood Pellets
Shrinkage start temp 980-1080°C

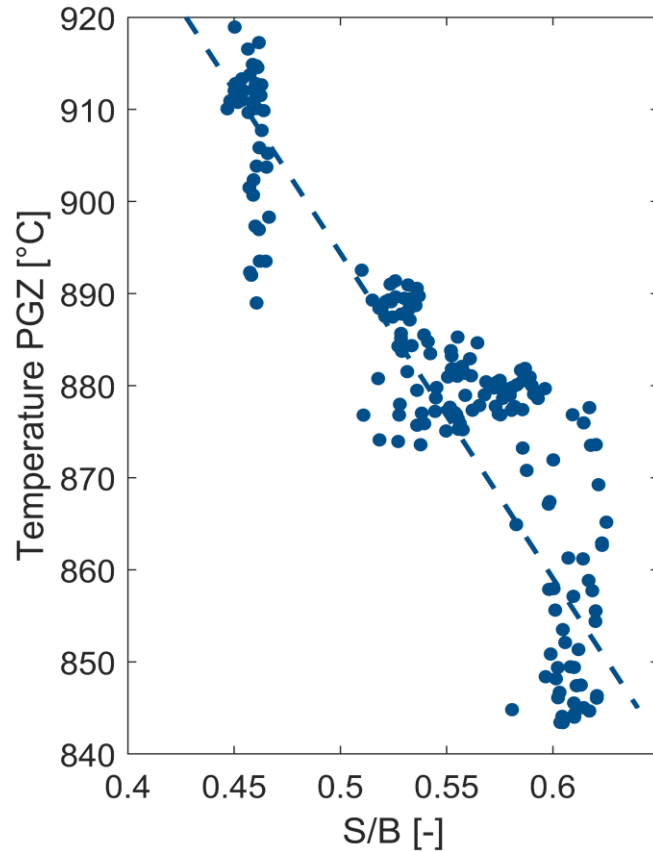


Heat up

Gasification

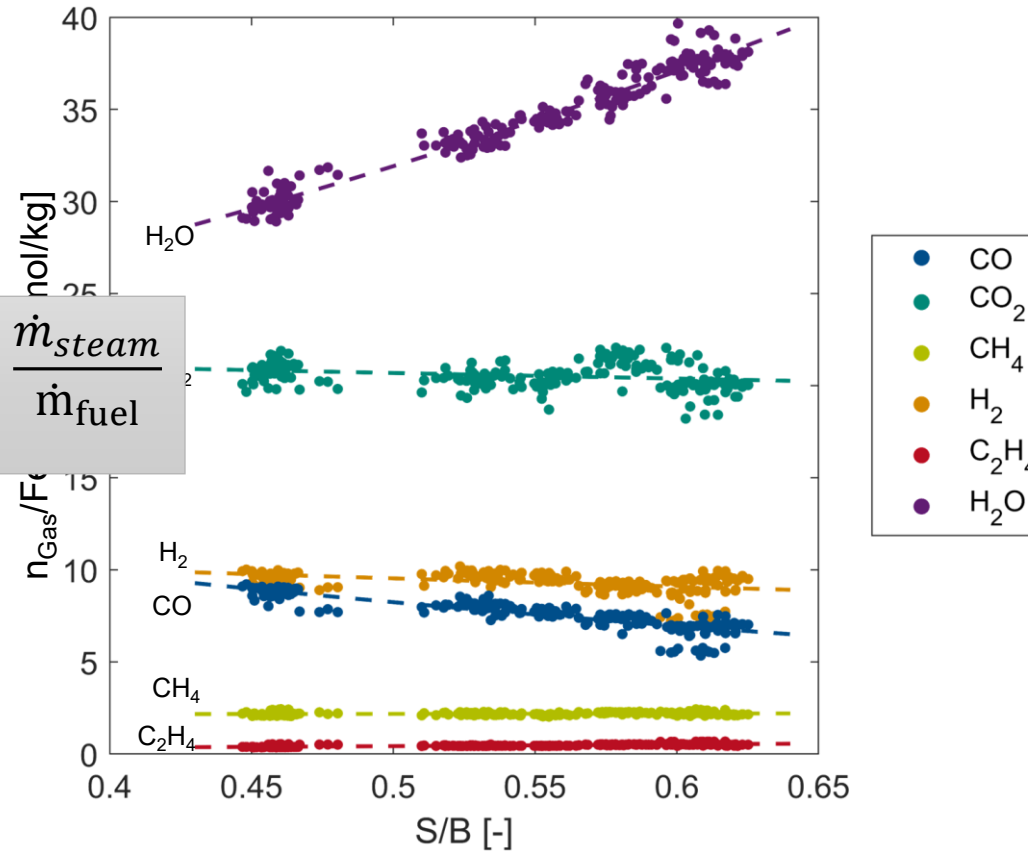
variation Steam to Biomass ratio

Influence Steam to Biomass Ratio



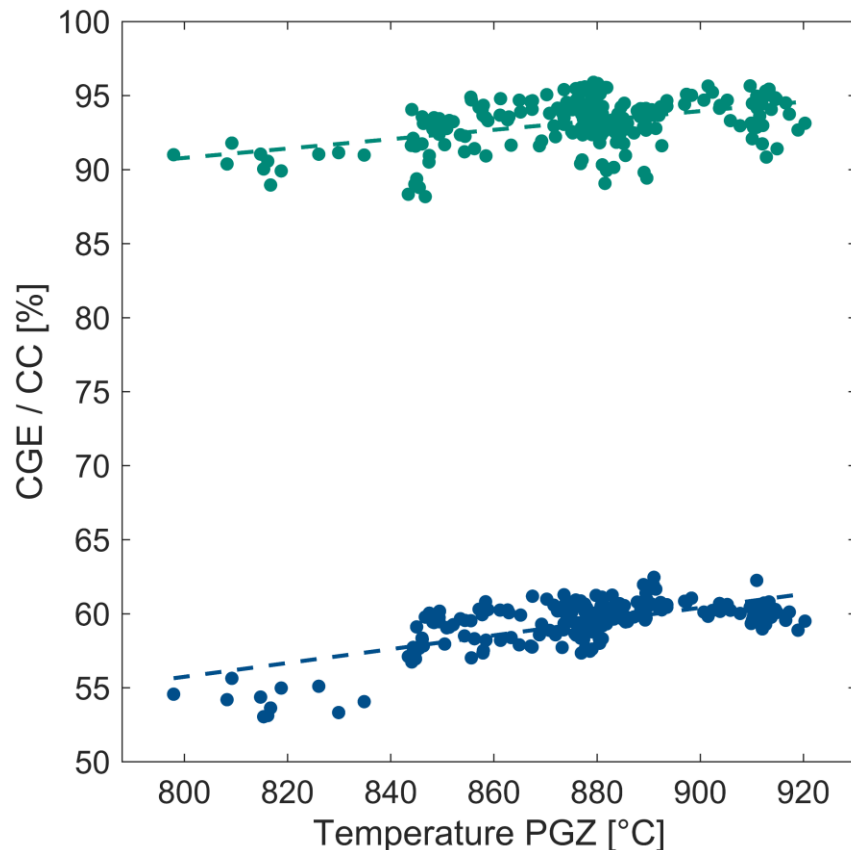
Thermal load: 430 kW_{th}
Lambda: 0.34

$$S/B = \frac{\dot{m}_{steam}}{\dot{m}_{fuel}}$$



NOTE: The higher CO₂ content in syngas compared to a commercial pressurized HTW® facility is mainly due to greater heat losses and lower gasification agent temperatures at the TU Darmstadt unit, requiring higher O₂ injection. In addition, the relative contribution of flushing CO₂ is higher at this small scale.

Cold Gas Efficiency and Carbon Conversion



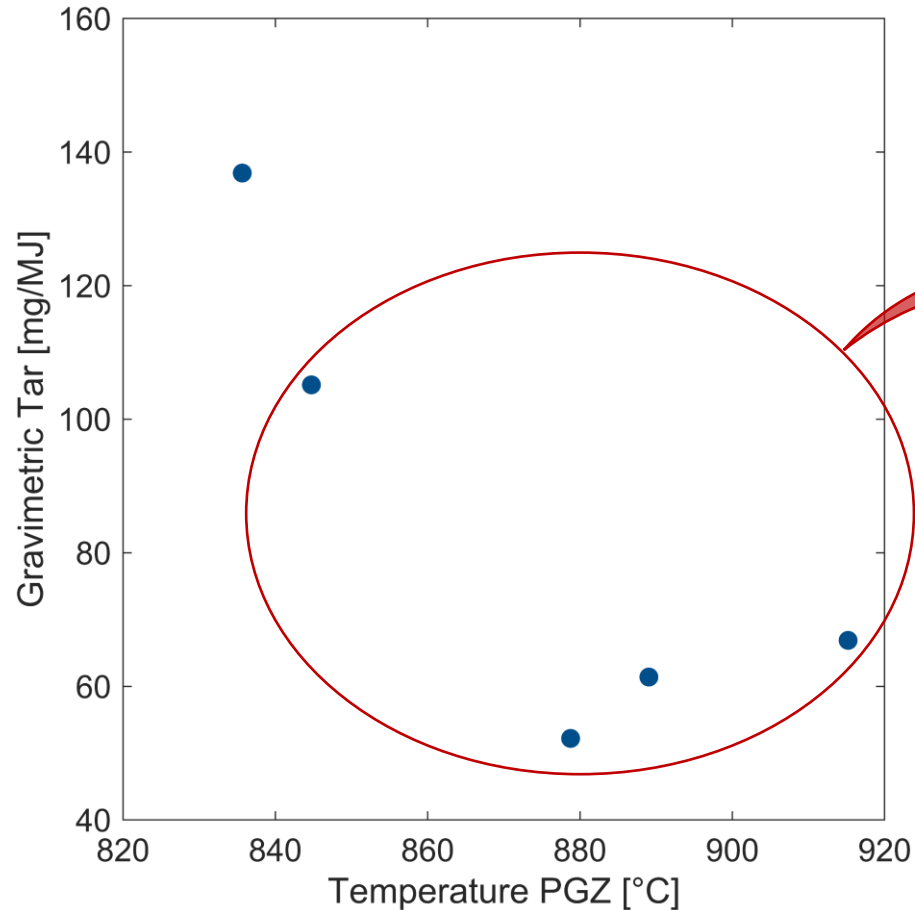
$$CGE = \frac{\sum \dot{m}_{j,syngas} * LHV_j}{\dot{m}_{fuel} * LHV_{fuel}}$$

with j H₂, CO, CH₄, C₂H₄

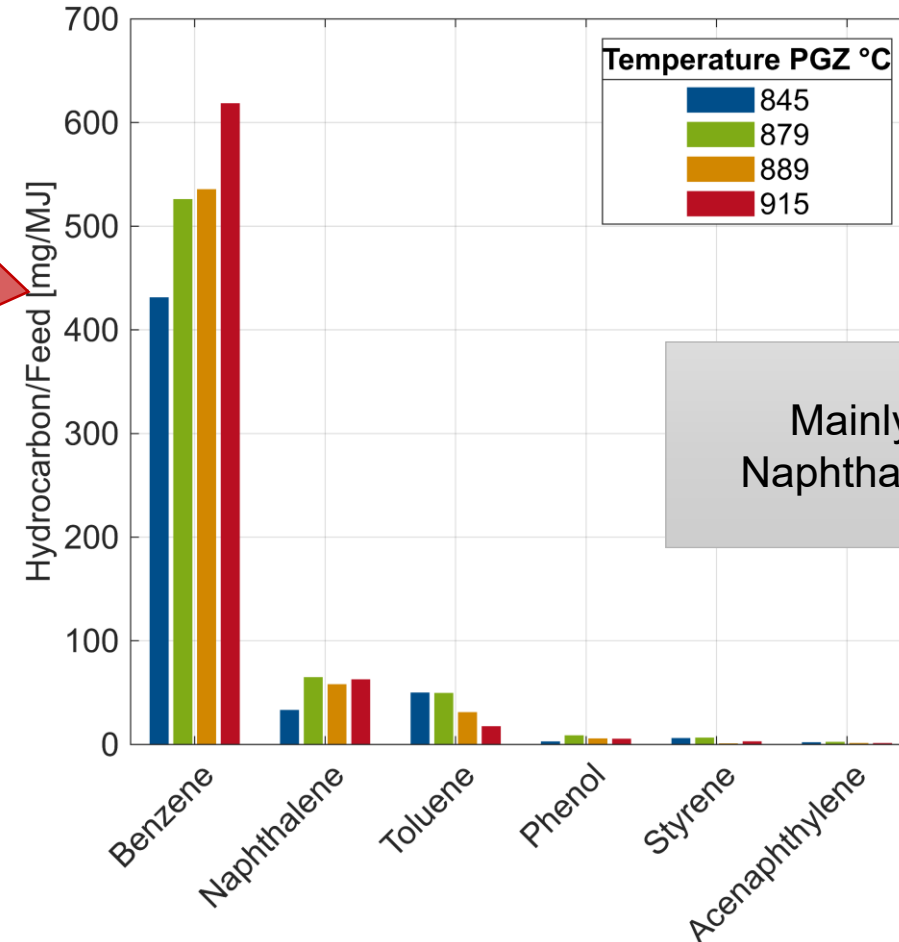
$$CC_{Gas} = \frac{\int_{t_0}^{t_1} \dot{n}_{c,syngas} dt}{\int_{t_0}^{t_1} \dot{n}_{c,fuel} dt}$$

Hydrocarbons

Gravimetric Tar



Detected hydrocarbons (GC)



Mainly Benzene,
Naphthalene, Toluene

Conclusion

✓ Proof of Concept: Waste Wood as Feedstock

- Stable process demonstrated for >100h using more than 8 tons feedstock
- Influence of reducing S/B
 - Enhances
 - Temperature, Syngas Yield, CC, CGE
 - Reduces
 - Long chain-hydrocarbons

⌚ Outlook

- Optimize lambda and S/B-ratio for an industrial gasifier
- Data is used for Life Cycle Assessment and 1D-Simulation
- Compare with chemical looping gasification

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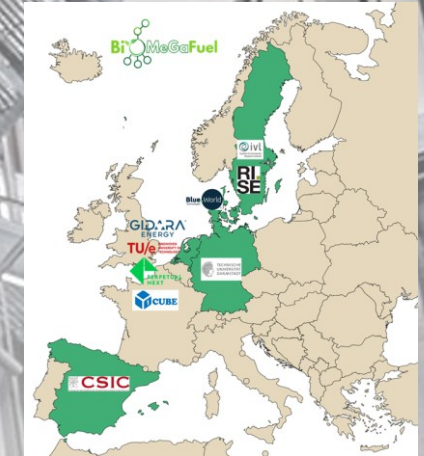
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THANK YOU



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EST HOMEPAGE

